

## Chapter 15

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- Time will permit us to focus only on venturi meter and pitot- static tube in class
- Common flowmeters are these + rotometer, magnetic, ultrasonic

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## Description of Venturi

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1. Meter constricts flow to narrow sections and then gradually expands again back to pipe diameter
2. Meter measures the pressure drop from pipe to the throat

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## How Venturi Works

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- Continuity says velocity increases
- Bernoulli says pressure drops
- Designed for minimal losses (no vena contracta). Losses would further increase the amount of pressure drop

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## Equations for Venturi

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- Losses taken into account with vendor supplying discharge coefficient C
- Text has Eq. 15-3, 4, & 5 incorrect on p. 442 and Eq 15-4 correct on p. 444

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## Corrected Equations for Venturi

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- To correct, substitute

$$\left(\frac{A_1}{A_2}\right)^2 - 1$$

- For

$$1 - \left(\frac{A_1}{A_2}\right)^2$$

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## Venturi Concluded

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- Discharge coefficient C is itself a function of the Reynolds number to about Re of 200,000

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## Description of Pitot-Static Tube

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- Static tube is a hollow tube (closed in front, with holes on side) that sees the pressure of the moving fluid
- Pitot tube is a hollow tube (with opening in front) that sees the pressure at the opening where the fluid has stopped moving

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## More Description

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- Tubes are concentric (central tube is the pitot) and connected to a differential manometer

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## How Pitot-Static Tube Works

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- Write Bernoulli from moving fluid to stagnation point, where  $v$  is local velocity

$$\frac{P_1}{\gamma} + \frac{v^2}{2g} = \frac{P_s}{\gamma} \quad \text{or } v = \sqrt{\frac{2g(P_s - P_1)}{\gamma}}$$

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## Confusing Terms in Pitot-Static Tube Equation

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- $P_1$  called static pressure even though fluid is moving
- $P_1/\gamma$  called static head even though fluid is moving
- $P_s$  = stagnation or total pressure at point of zero velocity

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## Drawbacks with Pitot-Static

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- To get average velocity, must take several readings at different points across the cross section of the pipe, and compute average velocity
- This is big drawback, which is why strap-on ultrasonic flowmeter has become so popular

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## Guidelines for Mounting Flow Meter

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For laminar, Length = ideally  $0.06 (Re) D$  from flow disturbance.

-For  $Re = 20$ ,  $L = D$ .

-For  $Re = 2300$ , this is  $138D$

Difficult to do in pilot plant

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## More Guidelines

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For turbulent, Length = about 4.4  
 $D (Re)^{1/6}$

For  $Re = 4000$ ,  $L = 18D$

For  $Re = 10^6$ ,  $L = 44D$

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## More Guidelines

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- Place where no boiling can occur and there's no entrained air.
- Place where your sure pipe is always full; i.e, mount in vertical pipe

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## What Goes Wrong with Flowmeters

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- Mounting problems previously discussed
- Flow is above range or below accurate range of flowmeter
- Usually no way to calibrate absolutely

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## More on What Goes Wrong with Flowmeters

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- Doesn't read zero at zero flow because electronics drift, etc
- Instrument people do only partial calibration at one value

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## Accuracy of Flowmeters

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- In typical chemical or paper plant, most accurate flow known is amount of product.
- Large flows can only be determined within + or - 20%, small flows + or - 10%
- If two flowmeters near the same point along a pipe read almost identical values, assume they are both wrong. Verify with other material balances.

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